

Efficient Electroreduction of Low Nitrate Concentration via Nitrate Self-Enrichment and Active Hydrogen Inducement on the Ce(IV)-Co₃O₄ Cathode

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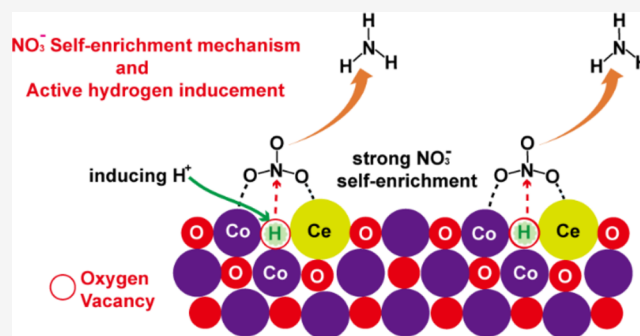
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ABSTRACT: Low concentrations of nitrate (NO_3^-) widely exist in wastewater, post-treated wastewater, and natural environments; its further disposal is a challenge but meaningful for its discharge goals. Electroreduction of NO_3^- is a promising method that allows to eliminate NO_3^- and even generate higher-value NH_3 . However, the massive side reaction of hydrogen evolution has raised great obstacles in the electroreduction of low concentrations of NO_3^- . Herein, we present an efficient electroreduction method for low or even ultralow concentrations of NO_3^- via NO_3^- self-enrichment and active hydrogen (H^*) inducement on the Ce(IV)-Co₃O₄ cathode. The key mechanism is that the strong oxytropism of Ce(IV) in Co₃O₄ resulted in two changes in structures, including loose nanoporous structures with copious dual adsorption sites of Ce–Co showing strong self-enrichment of NO_3^- and abundant oxygen vacancies (O_{vs}) inducing substantial H^* . Ultimately, the bifunctional role synergistically promoted the selective conversion of NH_3 rather than H_2 . As a result, Ce(IV)-Co₃O₄ demonstrated a NO_3^- self-enrichment with a 4.3-fold up-adsorption, a 7.5-fold enhancement of NH_3 Faradic efficiency, and a 93.1% diminution of energy consumption when compared to Co₃O₄, substantially exceeding other reported electroreduction cathodes for NO_3^- concentrations lower than 100 $\text{mg}\cdot\text{L}^{-1}$. This work provides an effective treatment method for low or even ultralow concentrations of NO_3^- .

KEYWORDS: self-enrichment, active hydrogen, Ce(IV)-Co₃O₄, low nitrate concentrations, electroreduction



INTRODUCTION

The natural nitrogen cycle is significantly affected by human activities, especially the wide distribution of nitrate (NO_3^-) in water bodies,^{1–3} which is the main cause of photochemical smog, methemoglobinemia, and cancer.^{4–6} Hence, further disposal of NO_3^- from water is becoming progressively critical. On the other hand, ammonia (NH_3) is not only an ideal, zero-carbon energy carrier in sustainable energy systems but also an essential feedstock for industrial production.^{7–9} Researchers have been investigating new NH_3 synthetic approaches under mild reaction conditions to overcome the large energy consumption and carbon emission issues of the Haber–Bosch process.^{10–13} Among various ammonia synthesis technologies, the electrochemical NO_3^- reduction reaction (NO_3RR), powered by renewable energy sources, uses electrons as a reducing agent with high efficiency and greenness that allows to simultaneously eliminate NO_3^- and generate NH_3 .^{14–19}

The reports about the electroreduction NO_3^- to NH_3 has significantly increased over the last 5 years with the catalyst designs focusing on the NH_3 yield,²⁰ NH_3 selectivity,²¹ and

current density.²² Nonetheless, most of those reported studies pay close attention to relatively concentrated NO_3^- (>100 mM or 1400 $\text{mg}\cdot\text{L}^{-1}$ NO_3^-/N),^{23–28} which are beneficial for efficient reactant mass transfer near the catalyst–electrolyte interface²⁹ and inhibition of the hydrogen evolution reaction (HER) side reaction.^{24,30} However, the electrochemical reduction of high concentrations of NO_3^- faces the problem of decrease in NO_3^- concentration, of which these water with diluted NO_3^- still cannot meet the discharge requirements.^{31,32} Hence, substantial energy is required to concentrate the low concentrations of NO_3^- around the cathodic surface for further treatment,³³ greatly affecting the practical application. For instance, palladium (Pd) has previously been demonstrated with the capability of electro-reducing NO_3^- to NH_3 , while at

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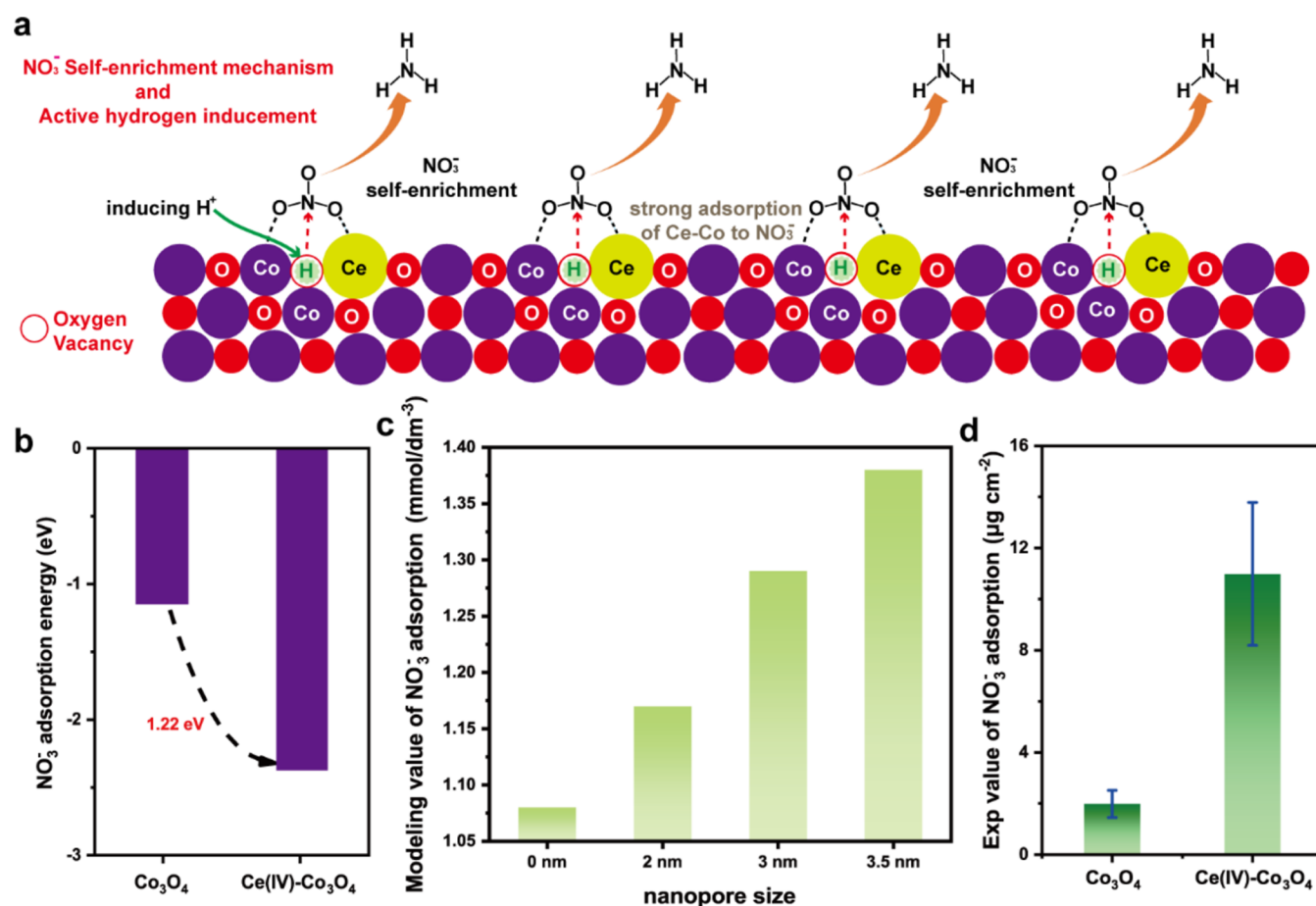


Figure 1. (a) Schematic mechanism of the self-enrichment and active hydrogen proliferation via $\text{Ce(IV)-Co}_3\text{O}_4$. (b) Calculated NO_3^- adsorption energies at the Co–Co dual site of Co_3O_4 and the Ce–Co dual site of $\text{Ce(IV)-Co}_3\text{O}_4$. (c) Simulated concentrations and distributions of local NO_3^- on the $\text{Ce(IV)-Co}_3\text{O}_4$ nanosheet surface for different pore size structures at 5 μs . The value of 3.5 nm was the maximum pore size of the constructed model, and the maximum concentration value from the simulation results was taken as the local NO_3^- concentration. (d) Actual adsorption of Co_3O_4 and $\text{Ce(IV)-Co}_3\text{O}_4$ at 1 mM-NO_3^- .

low NO_3^- concentrations ($<100 \text{ mg}\cdot\text{L}^{-1} \text{ NO}_3^-$ -N),²⁹ the Faradic efficiency (FE) and partial current density of producing NH_3 remain limited due to the poor adsorption of NO_3^- on Pd.^{34,35} Moreover, the typical abundance of NO_3^- concentrations in common wastewater, post-treated wastewater, or natural environments is low, e.g., seven $\sim 50 \text{ mg}\cdot\text{L}^{-1}$ (0.5–3.5 mM , Table S1). Even about 80% of industrial or agricultural polluted runoff has concentration of less than 10 $\text{mg}\cdot\text{L}^{-1}$ (ultralow concentrations),^{36,37} which still needs to be further reduced to meet the standard limit (Table S2). Thus, to achieve a reduction of low NO_3^- concentrations, it is necessary to address the enrichment and effective conversion around the electrode surface simultaneously.

Herein, we demonstrated the incorporation of CeO_2 and Co_3O_4 to form a $\text{CeO}_2/\text{Co}_3\text{O}_4$ nanocomposite (designated $\text{Ce(IV)-Co}_3\text{O}_4$) for the electroreduction of low concentrations of NO_3^- to NH_3 (Figure 1a). The strong oxytrophism of Ce(IV) in Co_3O_4 resulted in two changes of loose nanoporous structures and abundant oxygen vacancies (O_{vs}) in structures since the large radius of Ce distorted the lattice of Co_3O_4 , weakened the bond of Co–O, and engraved oxygen defect simultaneously. The positively charged dual sites of Ce–Co in loose nanoporous structures exhibited strong attraction to NO_3^- , realizing a higher enrichment for NO_3^- . The negatively charged centers of the O_{vs} activated H^+ to realize the

proliferation of active hydrogen (H^*). Ultimately, the bifunctional role between the NO_3^- self-enrichment and utilization of proliferative H^* makes it possible to selectively synthesize NH_3 rather than H_2 in low or even ultralow concentrations of NO_3^- . As results, $\text{Ce(IV)-Co}_3\text{O}_4$ exhibited superb performance over a wide NO_3^- concentration range (10–1000 $\text{mg}\cdot\text{L}^{-1} \text{ NO}_3^-$ -N); especially, it showed an excellent FE for nitrate reduction activity (NRA) of 92.3% and a low energy consumption (149.4 kWh/kg-N) in 10 $\text{mg}\cdot\text{L}^{-1} \text{ NO}_3^-$ solution, substantially exceeding those of pristine Co_3O_4 or Pd, and represented the highest reported data at low NO_3^- concentrations ($<100 \text{ mg}\cdot\text{L}^{-1} \text{ NO}_3^-$ -N). Hence, this work provides an effective method for the treatment of the NO_3^- water body, including high, low, or even ultralow concentrations.

MATERIALS AND METHODS

Chemicals. All chemicals were purchased from Sinopharm Chemical Reagent Co. Ltd. Deionized water was produced from a Millipore Milli-Q grade, with a resistivity of 18.2 $\text{M}\Omega\cdot\text{cm}$, and used for all experiments.

Synthesis of the $\text{Ce(IV)-Co}_3\text{O}_4$ /Copper Foam. The $\text{Ce(IV)-Co}_3\text{O}_4$ /copper foam was prepared via the reported method with a slight modification.³⁸ Prior to electrodeposition, copper foam (CF) was successively washed with ethanol and

dilute hydrochloric acid. The first was synthesized on the CF by electrodeposition from a solution of the corresponding metal nitrate(s) with a total concentration of 0.1 M. The synthesis of the Ce-doped $\text{Co}(\text{OH})_2$ precursor was as follows: 10 mol percent (mol %) of $\text{Co}(\text{NO}_3)_2$ in the solution was replaced with $\text{Ce}(\text{NO}_3)_3$, Ag/AgCl was the reference electrode, Pt mesh was the counter electrode, and a constant potential of -1.0 V vs Ag/AgCl was applied on the substrates for 10 min. After electrodeposition, the Ce-doped $\text{Co}(\text{OH})_2$ precursors were placed inside a tube furnace and then heated at 400°C for 2 h under a N_2 atmosphere. The obtained products were denoted as Ce(IV)- Co_3O_4 /CF, of which the model structure of Ce(IV)- Co_3O_4 is provided in Figure S1. For the synthesis of different percentages of Ce in Co_3O_4 /CF, different percents of Ce in Co_3O_4 /CF were obtained with the same method, but different mol percents (mol %) of $\text{Co}(\text{NO}_3)_2$ in the solution were replaced with $\text{Ce}(\text{NO}_3)_3$.

Synthesis of Co_3O_4 /CF and CeO_2 /CF. The synthesis of the $\text{Co}(\text{OH})_2$ and $\text{Ce}(\text{OH})_3$ precursors was performed according to the synthesis of Ce(IV)- Co_3O_4 /CF; solutions with only 0.1 M $\text{Co}(\text{NO}_3)_2$ solution and 0.1 M $\text{Ce}(\text{NO}_3)_3$ solution were used. After electrodeposition, the precursors were placed inside a furnace and then heated to 400°C for 2 h. The obtained products were denoted as Co_3O_4 /CF and CeO_2 /CF.

Other detailed methods are provided in the Supporting Information.

RESULTS AND DISCUSSION

Catalyst Characterization. Ce(IV)- Co_3O_4 was prepared by the in situ electrodeposition of Ce- $\text{Co}(\text{OH})_2$, followed by thermal annealing. X-ray diffraction (XRD) was applied to detect the crystalline structures of Ce(IV)- Co_3O_4 . Figure S2a shows that the obvious diffraction peaks were mainly attributed to Co_3O_4 signals, and a CoO peak clearly appeared on Co_3O_4 and Ce(IV)- Co_3O_4 .^{38,39} In addition, the tiny diffraction of CeO_2 ($\sim 28.5^\circ$) was observed in the XRD owing to the low Ce content in the sample.³⁸ Figure S2b displays the results of Fourier transform infrared (FTIR) spectroscopy. In addition to the evident peak at ~ 566 and 644 cm^{-1} corresponding to the Co–O bond on Ce(IV)- Co_3O_4 and Co_3O_4 ,⁴⁰ the Ce–O stretching vibration located at $\sim 1060\text{ cm}^{-1}$ was attributed to the formation of CeO_2 on Co_3O_4 ,⁴¹ suggesting that the successful introduction of CeO_2 into Co_3O_4 .

Scanning electron microscopy (SEM) images showed that Ce(IV)- Co_3O_4 nanosheets with petal shapes were homogeneously deposited on the copper foam surface. The average nanosheet sizes were $\sim 200\text{ nm}$ (Figure S3), with abundant loose nanopores on the nanosheets (Figure S4). Atomic force microscopy (AFM) study showed that the thickness of Ce(IV)- Co_3O_4 was determined to be $\sim 3.6\text{ nm}$ (Figure S5a). Transmission electron microscopy (TEM) images showed the lamellar structure of Ce(IV)- Co_3O_4 (Figure S5b). Energy-dispersive X-ray spectroscopy (EDS) elemental mappings confirmed the uniform distributions of Co, Ce, and O elements across the whole sample, in which the atomic ratio of Ce and Co was $\sim 1:10$ (Figure S5c). High-resolution TEM (HRTEM) images showed visible lattice spacings of 0.240, 0.286, and 0.310 nm (Figure S5d), corresponding to the CoO (200), Co_3O_4 (220), and CeO_2 (111) planes.³⁹ These results confirmed that CeO_2 was successfully introduced into Co_3O_4 . Many interfacial vacancies were observed on the CeO_2 and Co_3O_4 interface (Figure S5e).

Additionally, X-ray photoelectron spectroscopy (XPS) was conducted to investigate the chemical status of Co and O (Figure S6). The high-resolution O 1s and Co 2p spectra of Co_3O_4 and Ce(IV)- Co_3O_4 are shown in Figure S7a,b. The presence of Co^{2+} and Co^{3+} was observed on both Co_3O_4 and Ce(IV)- Co_3O_4 and deconvoluted into four peaks.⁴² Ce(IV)- Co_3O_4 contained a higher $\text{Co}^{2+}/\text{Co}^{3+}$ ratio ($\sim 45/55$) than Co_3O_4 ($\sim 30/70$), suggesting the higher content of Co^{2+} and the existence of a fraction of oxygen vacancies (O_{vs}).^{39,43} As shown in Figure S7b, the oxygen species of the surface hydroxyl groups ($-\text{OH}$), lattice oxygen (O_{L}), and O_{vs} were present on the surface of the catalyst.⁴⁴ Ce(IV)- Co_3O_4 exhibited a much higher O_{v} fraction (48%) than Co_3O_4 (11%), which was potentially due to the stronger interaction between Ce and O in Ce(IV)- Co_3O_4 .⁴⁵ The Raman spectra of Co_3O_4 and Ce(IV)- Co_3O_4 are displayed in Figure S7c. The characteristic Raman peaks were located at approximately 680, 516, and 475 cm^{-1} , corresponding to the typical Raman-active modes of $\text{A}_{1\text{g}}$, $\text{F}_{2\text{g}}$, and $\text{E}_{2\text{g}}$.⁴⁶ Note that the $\text{A}_{1\text{g}}$ peak of Ce(IV)- Co_3O_4 shifted to a higher frequency than that of Co_3O_4 , which signified the change in the long-range order of the crystal, indicating the formation of the O_{vs} . Furthermore, Ce(IV)- Co_3O_4 showed a stronger signal ($g = 2.006$) of electron paramagnetic resonance (EPR) compared with Co_3O_4 (Figure S7d). This result was associated with the vacancy center and further confirmed the amplification of O_{vs} in Ce(IV)- Co_3O_4 .⁴⁷ Thus, introducing Ce atoms could regulate the microstructure and improve the Co^{2+} content by weakening the bond of Co and O to induce loose nanoporous structure and amplify O_{vs} .

Theoretical Analysis. To get an understanding of NO_3RR via Ce(IV)- Co_3O_4 , the structure–activity relationship was investigated. At low NO_3^- concentration, the competitive adsorption of H_2O leads to the occurrence of H–H dimerization, resulting in the production of H_2 and a decrease of the Faradic efficiency (FE) for NO_3RR .⁴⁸ Hence, the better NO_3^- enrichment on the catalyst could obviously inhibit the H–H dimerization. First, the density functional theory (DFT) calculations were applied to conduct the NO_3^- and H_2O adsorption free energies on the Ce and Co sites. In Figure S8a, Ce(IV)- Co_3O_4 required -0.97 eV of H_2O adsorption energy, which is much more positive than the NO_3^- adsorption energy (-2.37 eV) with the gap of 1.40 eV , while the gap of adsorption energy between H_2O and NO_3^- on Co_3O_4 was 0.81 eV (Figure S8b), which indicated that introducing Ce ions into Co_3O_4 can suppress the negative impact of H_2O . Figure 1b shows the adsorption energies of NO_3^- on the Co–Co dual site and the Ce–Co dual site in Co_3O_4 and Ce(IV)- Co_3O_4 , respectively. Notably, Ce(IV) had an extremely strong affinity for oxygen of NO_3^- , in which the Ce–Co dual site (-2.37 eV) showed a more negative adsorption energy than the Co–Co dual site (-1.05 eV), meaning the preferential NO_3^- adsorption on the Ce(IV)- Co_3O_4 catalyst. Comparing the adsorption energy of NO_3^- on other sites of Ce(IV)- Co_3O_4 (Figure S9), it was found that the Ce–Co dual site indeed exhibited the best adsorption capacity.

On the other hand, COMSOL Multiphysics was utilized to simulate the electric field distribution around the surface under different morphologies (Figure S10). A denser electric field distribution in the electrode region indicated that the geometry of the loose nanopores greatly increased the specific capacity, thus expanding the NO_3^- reduction.⁴⁹ Subsequently, finite element method (FEM) analysis was applied to simultaneously simulate the local concentration of NO_3^- around Co_3O_4 and

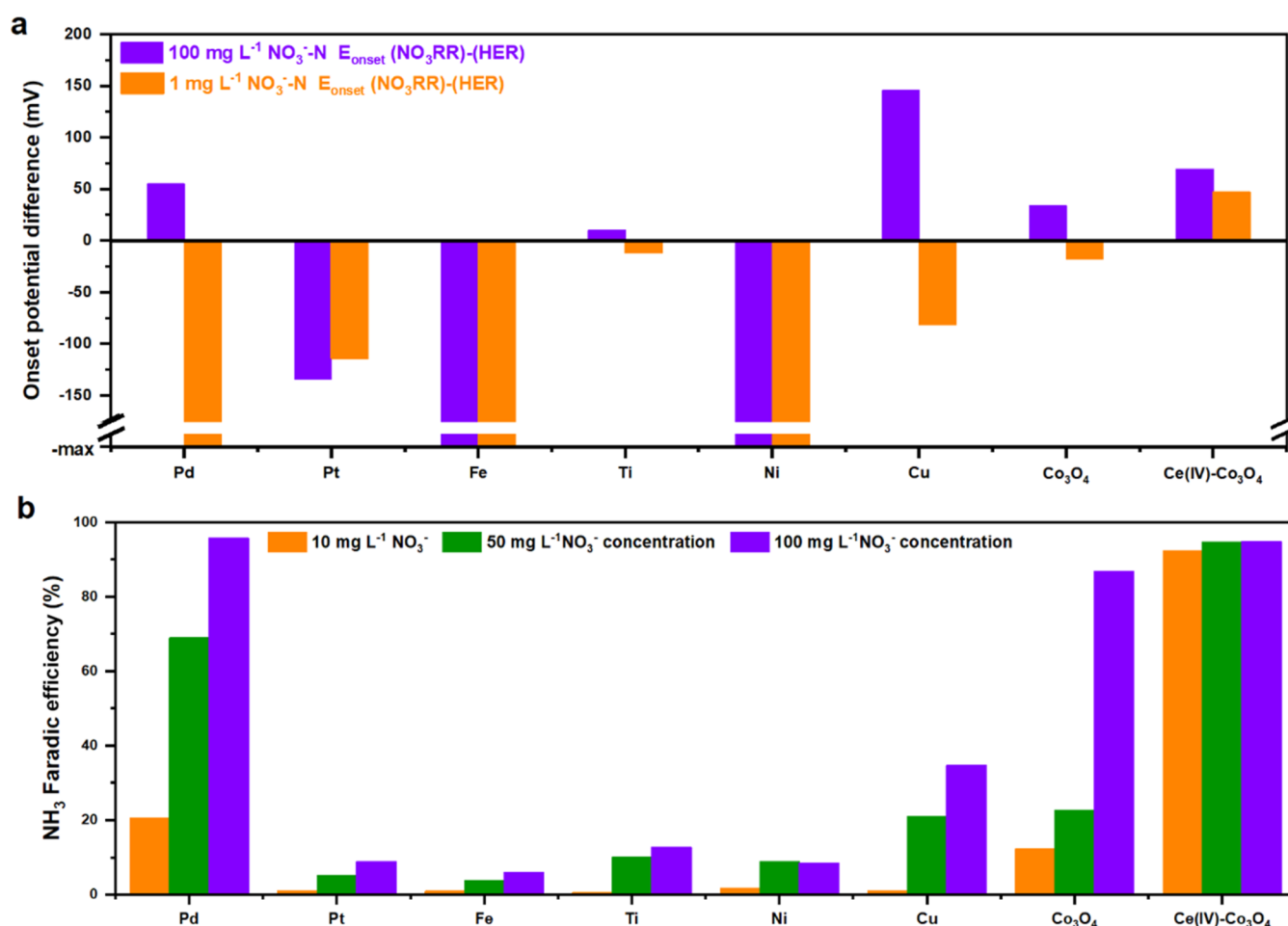


Figure 2. Catalysts with a distinctive electrocatalytic preference between the NO₃⁻ reduction reaction (NO₃RR) and hydrogen evolution reaction (HER). (a) Onset potential difference between the NO₃⁻ reduction reaction and HER: “E_{onset}(NO₃RR) – E_{onset}(HER)”. –max means only HER proceed. LSV curves of the different catalysts in three different solutions: 0.1 M Na₂SO₄ (black curve) and 0.1 M Na₂SO₄ with 1–100 mg·L⁻¹ NO₃⁻. A scan rate of 10 mV·s⁻¹ was used for LSV on all catalysts. The geometric area of catalyst was 1 cm². (b) NH₃ Faradic efficiency difference between NO₃⁻ electroreduction to NH₃. The FEs obtained by converting the half concentration of NO₃⁻ to NH₃ for comparison.

Ce(IV)-Co₃O₄. With the diffusion, more NO₃⁻ accumulated on the surface of Ce(IV)-Co₃O₄ (Figure S11a), while little NO₃⁻ migrated to the surface of Co₃O₄ (Figure S11b) owing to the self-enrichment of Ce(IV)-Co₃O₄. As the simulated results show in Figure 1c, in nanoporous structure, the enrichment increases with the expansion of pore size, although the enhancement amplitude weakened when the pore size exceeded 3 nm. We further detected the adsorption quantity of the different catalysts at a concentration of 1 mM·NO₃⁻ (Figure 1d) and found that the adsorption quantity of Ce(IV)-Co₃O₄ was 4.3 times that of Co₃O₄, which showed similar tendencies. These findings indicated that the presence of a Ce–Co dual site in the loose nanoporous structure self-enriched NO₃⁻.

Catalytic Performance. The onset potentials of both the NO₃RR and HER were obtained from linear sweep voltammetry (LSV). The more positive onset potential difference was defined as ΔE_{onset}, which is “E_{onset}(NO₃RR) – E_{onset}(HER)”. Figure 2a illustrates the excellent performance of Ce(IV)-Co₃O₄ in NO₃⁻ reduction with the positive ΔE_{onset} of 69 mV, of which the onset potential difference was close to that of Pd (55 mV). Note that Pd has previously been reported as the best catalyst in NO₃⁻ electroreduction.^{19,50–53} The Ce(IV)-Co₃O₄ catalyst exhibited performances comparable to

Pd for NO₃RR in the presence of a high concentration of NO₃⁻ (100 mg·L⁻¹ NO₃⁻-N) (Figures S12a and S13a). At a concentration of NO₃⁻ lower than 100 mg·L⁻¹, Pd and other catalysts were unable to reduce NO₃⁻ (Figure S12), in which the onset potential differences (ΔE_{onset}) were all negative. For comparison, Ce(IV)-Co₃O₄ exhibited superior NO₃RR (ΔE_{onset}: 47 mV) even at extremely low NO₃ concentrations (1 mg·L⁻¹) (Figures S12h and S13c), suggesting its promising potential for NRA at a low concentration of NO₃⁻. The FEs of the above catalytic materials for electroreduction to NH₃ at different NO₃⁻ concentrations is shown in Figure 2b and Table S3. Obviously, Pd, Co₃O₄, and Ce(IV)-Co₃O₄ all exhibited the best FE at high concentrations of NO₃⁻ (>1000 mg·L⁻¹ NO₃⁻-N). However, only Ce(IV)-Co₃O₄ still maintained superior FE at low NO₃⁻ concentrations (10–50 mg·L⁻¹ NO₃⁻-N), while other two cathodes showed a cliff-like drop when the concentration decreased due to the side reaction of hydrogen evolution.

To further investigate the catalytic performance of Ce(IV)-Co₃O₄ for NRA, the surface areas of the catalysts were measured. As shown in Figure S14, Ce(IV)-Co₃O₄/CF (372 cm² ECSA) had a higher electrochemical surface area (ECSA) than CF (32 cm² ECSA) and Co₃O₄/CF (292 cm² ECSA), resulting in a positive impact on the NO₃RR. In addition, the

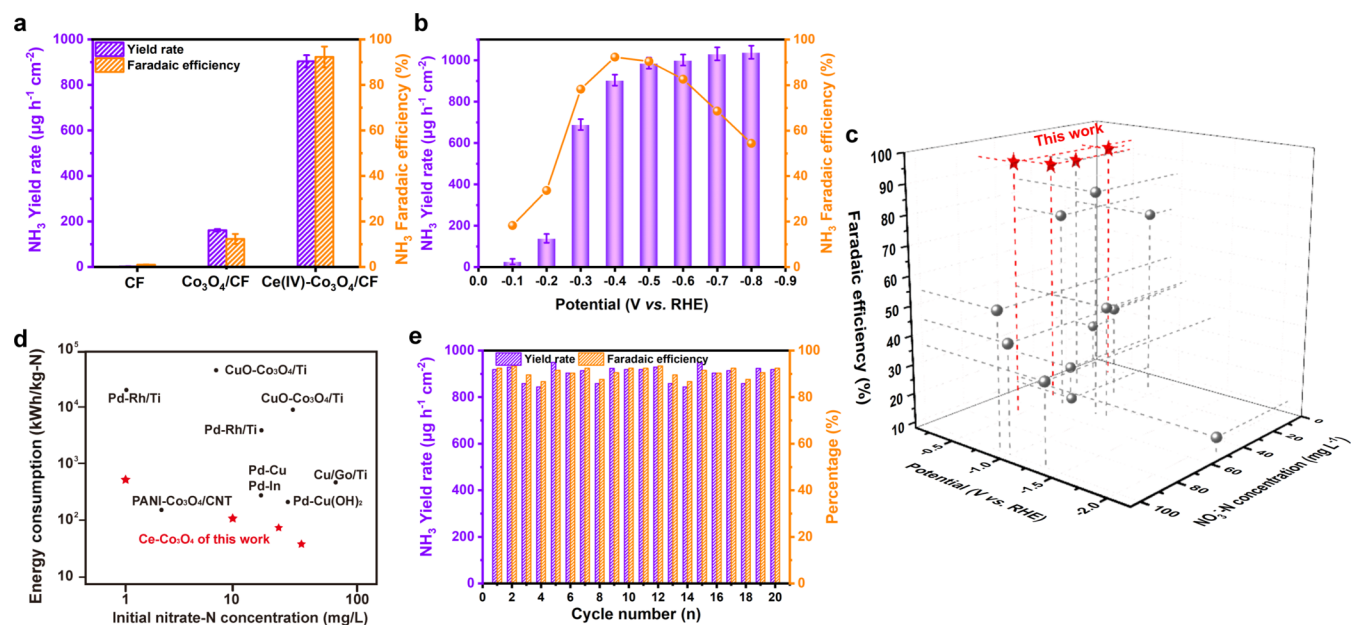


Figure 3. (a) NH₃ yield rate and Faradic efficiency over NO₃⁻ in (a) different samples and (b) applied potentials. (c) Comparison of the performance of Ce(IV)-Co₃O₄ with other reported catalysts. Red star represents the performance of this work. (d) Energy consumption of the reported electrochemical nitrate reduction studies in a low concentration of NO₃⁻ via one-step reduction. Starting nitrate concentrations and the corresponding energy consumptions (kWh/kg-N) in the reported electrochemical nitrate reduction studies. (e) Consecutive recycling test at -0.4 V for Ce(IV)-Co₃O₄/CF with 10 mg·L⁻¹ NO₃⁻ for 20 min.

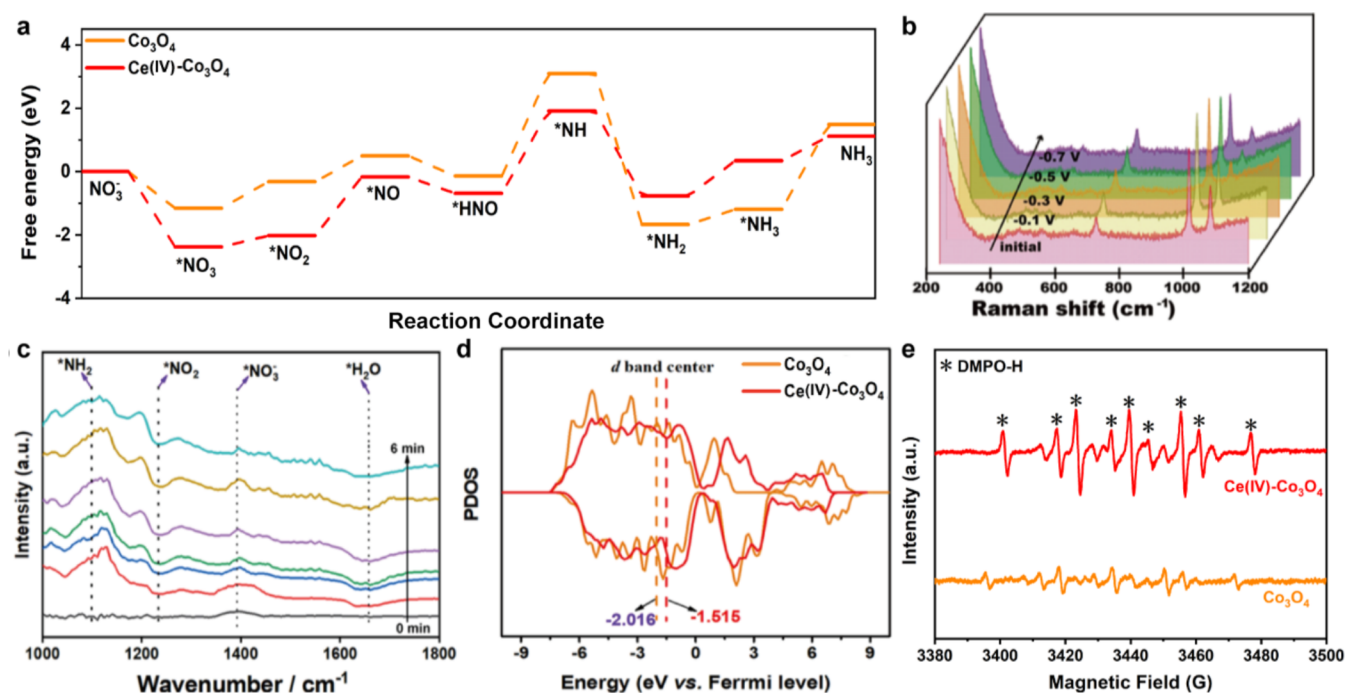


Figure 4. (a) Calculated free energy of the NRA process on Co₃O₄ and Ce(IV)-Co₃O₄. (b) *In situ* Raman spectra at different applied potentials vs RHE. (c) *In situ* FTIR spectra of Ce(IV)-Co₃O₄ under -0.4 V vs RHE with 10 mg·L⁻¹ NO₃⁻. (d) PDOS of *d*-bands for Co₃O₄ and Ce(IV)-Co₃O₄ and the corresponding *d*-band centers. (e) DMPO spin-trapping ESR spectra of Co₃O₄ and Ce(IV)-Co₃O₄.

Brunauer–Emmett–Teller (BET) surface areas for Co₃O₄ and Ce(IV)-Co₃O₄ were analyzed (Figure S15a). The surface area of Ce(IV)-Co₃O₄ was 8.01 m²·g⁻¹, which was also 6.2 times higher than that of Co₃O₄ (1.29 m²·g⁻¹) (Table S4), indicating that the nanoporous structure (10–30 nm) was constructed via the oxyphilic effect of Ce(III) to Ce(IV) (Figure S15b). The cyclic voltammetry (CV) curves with a wider potential range are shown in Figure S16, in which the specific capacity

was enhanced with the introduction of Ce.⁵⁴ The capacitive contribution of NO₃⁻ in the double electric layer of Ce(IV)-Co₃O₄ led to the steep characteristic peak at 0.13 V.⁵⁵ The Nyquist plots of Ce(IV)-Co₃O₄/CF, Co₃O₄/CF, and CF were obtained via electrochemical impedance spectroscopy (Figure S17), where a smaller arc radius meant lower charge transfer resistance and faster interfacial electron transfer,⁵⁶ suggesting the high intrinsic activity of Ce(IV)-Co₃O₄.

Furthermore, the above electrodes were used to test the NRA performance at low concentrations of NO_3^- ($10 \text{ mg}\cdot\text{L}^{-1}$ NO_3^- -N and $0.1 \text{ M Na}_2\text{SO}_4$) using a three-electrode system, in which the variations of nitrogen compounds were detected by ultraviolet–visible (UV/vis) absorbance spectra (Figure S18). As shown in Figure 3a, Ce(IV)- Co_3O_4 /CF showed the best performance of NH_3 yield rate ($904 \mu\text{g}\cdot\text{h}^{-1}\cdot\text{cm}^{-2}$) and NH_3 FE (92.3%), better than Co_3O_4 /CF (NH_3 FE: 12.3%, NH_3 yield rate: $161 \mu\text{g}\cdot\text{h}^{-1}\cdot\text{cm}^{-2}$) and CF (NH_3 FE: 1.0%, NH_3 yield rate: $2.02 \mu\text{g}\cdot\text{h}^{-1}\cdot\text{cm}^{-2}$). The performance of Ce(IV)- Co_3O_4 was further tested under different applied potentials (Figure 3b). The NH_3 yield rate showed growth as the potential became more negative from -0.1 to -0.8 V vs RHE, while the NH_3 FEs displayed a volcanic trend, which were also much better than those reported by other catalysts (Table S5 and Figure 3c). Thereafter, the catalytic ability of Ce(IV)- Co_3O_4 /CF showed a high level in an extremely high concentration of NO_3^- ($1000 \text{ mg}\cdot\text{L}^{-1}$ NO_3^- -N; Figure S19). Indeed, an energy analysis (Table S6) revealed that the energy consumption of Ce(IV)- Co_3O_4 (149.4 kWh/kg-N) was much lower than that of Co_3O_4 (2180.2 kWh/kg-N) and also outperformed previous reports of using Pd-based and other catalysts (Figure 3d).^{37,57–60} Figure S20 shows the variation in NO_3^- , NO_2^- , and NH_3 without the detection of N_2 during the NRA reaction with time. NO_3^- dramatically decreased over 20 min using the Ce(IV)- Co_3O_4 /CF electrode and 99.1% of NO_3^- was converted to NH_3 , which showed the good NH_3 selectivity. As shown in Figure S21, the FEs of side reactions of H_2 and NO_2^- generation were 6.7% and 0.9%, respectively. After 20 consecutive recycling runs using Ce(IV)- Co_3O_4 (Figure 3e), both the NH_3 yield rate and FEs showed negligible decline, the dissolved Ce and Co ions of Ce(IV)- Co_3O_4 during NO_3RR in electrolyte was negligible (Figure S22), and among the morphology, lamellar structure and valence states were preserved after the electrolysis (Figure S23), confirming the excellent stability and robustness of Ce(IV)- Co_3O_4 .

Mechanistic Studies. To gain further insight into the NRA capability of Ce(IV)- Co_3O_4 , DFT calculations and experiments were conducted. *In situ* Raman spectra (Figure S24a) showed peaks at approximately 1050 and 980 cm^{-1} , which were assigned to NO_3^- and SO_4^{2-} , respectively, and peaks at 688 and 462 cm^{-1} , which were attributed to the Co–O and O–Ce–O stretching vibration, respectively, indicating the valence states of Co(II) and Ce(IV).^{15,61} In Figure S24b, the peaks of Co–O in Co_3O_4 disappeared, indicating that Co(II) was converted into Co^0 , while the Co–O and O–Ce–O peaks in Ce(IV)- Co_3O_4 still existed, suggesting the stabilization of the Co intermediate because CeO_2 suppresses the reduction of Co(II) during electrocatalysis.³⁸ After that, the Gibbs free energies of each step (Figure 4a and Table S7) and the constructed models of Ce(IV)- Co_3O_4 for NRA (Figure S25) were displayed, in which Ce(IV)- Co_3O_4 reduced the reaction energy for the rate-determining step of $^*\text{HNO}$ to $^*\text{NH}$. Finally, the desorption step of NH_3 from $^*\text{NH}_3$ on Ce(IV)- Co_3O_4 required lower energy (0.77 eV) owing to the deoxygenation and hydrogenation processes altering the binding sites. Importantly, the plausible intermediate of $^*\text{NHO}$ or $^*\text{NOH}$ was compared in the calculation. However, free energy is -0.51 eV for $^*\text{NHO}$ and 0.21 eV for $^*\text{NOH}$ (Figure S26), indicating the intermediate of $^*\text{NHO}$ during NO_3RR . The Raman spectrum was identical when a more negative potential is applied in Ce(IV)- Co_3O_4 (Figure 4b), indicating that HER was not likely to occur. As shown in

electrochemical *in situ* attenuated total reflectance (ATR)-FTIR spectroscopy (Figure 4c), the asymmetric stretching vibration of NO_3^- appeared at 1392 cm^{-1} and the downward band at 1638 cm^{-1} , indicating the enrichment of NO_3^- and the generation of H^* for NO_3^- deoxygenation.⁶² The projected density of states (PDOS) associated with the electronic structure was calculated (Figure 4d), and the corresponding *d*-band centers of Co_3O_4 and Ce(IV)- Co_3O_4 were -2.016 and -1.515 eV vs the Fermi level. The right shift of the PDOS with the distribution of *d*-band electrons relatively closer to the Fermi level for Ce(IV)- Co_3O_4 indicated the adsorption for the critical intermediates of $^*\text{NO}_2$, $^*\text{NO}$, $^*\text{HNO}$, $^*\text{NH}$, and $^*\text{NH}_2$ by the NRA reaction (Figure S27). Furthermore, the formation of H^* was detected during the NRA reaction, in which 5,5-dimethyl-1-pyrroline-N-oxide (DMPO) was used as the quenching reagent. The signals of the nine characteristic peaks of DMPO-H ($1:1:2:1:2:1:2:1:1$) for Ce(IV)- Co_3O_4 were much stronger and clearer (Figure 4e), as more O_{vs} in Ce(IV)- Co_3O_4 strengthened the activation of H^+ into H^* . Note that in the presence of NO_3^- , the DMPO-H peaks of Ce(IV)- Co_3O_4 disappeared (Figure S28), suggesting that H^* was consumed for NRA reaction. The DFT calculation revealed that the required energy for Ce(IV)- Co_3O_4 (0.86 eV) to form H^* was much lower than that of Co_3O_4 (1.51 eV), also confirming the positive effect of the O_{vs} on H^* generation (Figure S29). The quenching experiments were applied to deeply identify the H^* role, in which *tert*-butyl alcohol (TBA) was used as the specific H^* quenching agent.¹⁰ The conversion of NO_3^- continuously decreased as the concentration of TBA was increased from 0 to 10 mM (Figure S30a,b). Moreover, Figure S31 intuitively shows the FEs at different Ce contents. Of these, excessive Ce (IV) entering Co_3O_4 significantly altered the distribution of O around Co to change the synergistic reactive performance of self-enrichment and O_{vs} amplification. Excessive Ce and O_{vs} could alter the structure of the nanosheets to affect the utilization of H^* and reduced the NH_3 FE, indicating the intrinsic activity of suitable equilibrium of NO_3^- self-enrichment and H^* production. Based on all of the theoretical calculations and experiments, the introduction of Ce ions were allowed to enrich NO_3^- , modulate the *d*-band center, and enhance the generation of H^* , thus leading to the highly selective reduction of low concentrations of NO_3^- to NH_3 .

ENVIRONMENTAL APPLICATION

The elimination of low concentrations of NO_3^- is essential, and converting it into higher-value NH_3 is a very attractive approach to validate a widely aqueous pollutant to valuable chemical feedstock. However, with the progress of electroreduction, H^* easily formed the H_2 overflow owing to the poor accessibility of NO_3^- on the cathodic surface at low concentrations of NO_3^- . In this work, the designed Ce(IV)- Co_3O_4 was fabricated by inserting CeO_2 into Co_3O_4 , featuring a bifunctional role: (1) the strong self-enrichment of NO_3^- via the efficient adsorption of the Ce–Co dual site and (2) the generation of O_{v} near the Ce–Co dual site to effectively generate H^* . Hence, the Ce(IV)- Co_3O_4 with excellent stability allowed to convert NO_3^- into NH_3 with a high NH_3 FE and a low energy consumption at a wide NO_3^- concentrations range, including low or even ultralow concentrations (10 – $1000 \text{ mg}\cdot\text{L}^{-1}$ NO_3^- -N), substantially exceeding previously reported catalysts including Pd-based catalysts. Even the electrochemical reduction of a high concentration of NO_3^- continuously

diluted with NO_3^- still maintained the electrocatalytic NRA, which expanded the application of the electrochemical NO_3^- treatment. Thereafter, actual water from different sources, including industrial wastewater, post-treated wastewater, and natural surface water, were collected to explore the application of the $\text{Ce(IV)}-\text{Co}_3\text{O}_4$ cathode. As shown in Table S8, NO_3^- , in all kinds of actual water bodies with a wide concentration range ($10\text{--}1000\text{ mg}\cdot\text{L}^{-1}\text{ NO}_3^-\text{-N}$), was effectively eliminated and further converted to NH_3 . Furthermore, consecutive recycling tests were used to evaluate the longevity of $\text{Ce(IV)}-\text{Co}_3\text{O}_4$ in actual surface water treatment. After consecutive recycling runs, the performance of NO_3^- elimination and NH_3 generation have no significant variation (Figure S32). As the reduction of NO_3^- consumed H^+ , the pH value increases during the reaction (Figure S33). In addition, different kinds of anions were added into the simulated solution to confirm the NO_3RR performance of $\text{Ce(IV)}-\text{Co}_3\text{O}_4$; obviously, different anions had almost no impact on the NO_3^- reduction of $\text{Ce(IV)}-\text{Co}_3\text{O}_4$ electrode (Figure S34). The costs compared to other catalysts were also investigated and are listed in Table S9, with $\text{Ce(IV)}-\text{Co}_3\text{O}_4$ showing the lowest cost of NH_3 production in all kinds of real wastewater treatments. Hence, our work provides a facile synthesis method for efficient NRA reactions at a wide NO_3^- concentration range and can facilitate an efficient strategy for treating wastewater with low concentrations of NO_3^- .

■ ASSOCIATED CONTENT

Supporting Information

The Supporting Information is available free of charge at <https://pubs.acs.org/doi/10.1021/acs.est.4c06263>.

Detailed experimental studies; simulated methods; computational methods; additional SEM and TEM images; XRD results; XPS spectra; electrochemical measurements; and quantification of products and DFT data (PDF)

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Notes

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